### Module 3a: Flow in Closed Conduits Continuity, Momentum, and Energy (Bernoulli)

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### **Equation of Continuity**

At any given location (**assuming incompressible fluid**): Flow In = Flow Out  $Q_{in} = Q_{out}$ Since Q = (Velocity)(Cross-Sectional Area of Flow) = VA

Where V = average (mean) velocity across the profile. (VA)<sub>in</sub> = (VA)<sub>out</sub>

#### **Continuity Equation**

Example:

Water flows in a 10-cm diameter pipe at a mean velocity of 1.5 m/sec. What is the discharge rate of flow at a temperature of 5°C?

Using the continuity equation,

Q = VA Substituting:

$$Q = (1.5m/\sec)\left(\frac{\pi}{4}\right)(0.10m)^2$$

 $Q = 0.012m^3 / \sec$ 

#### **Continuity Equation**

Example:

- Water flows in a 10-cm diameter pipe at a mean velocity of 1.5 m/sec. What is the discharge rate of flow at a temperature of 5°C?
- Had the example asked for the mass rate of flow, the mass rate of flow is equal to the flow Q multiplied by the density of the fluid at the temperature of interest.

Mass rate of flow =  $(0.012 \text{ m}^3/\text{sec})(1000 \text{ kg/m}^3)$ Mass rate of flow = 12 kg/sec

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## **Continuity Equation**

#### Example:

- Water is flowing in a 2-inch diameter pipe at a velocity of 16 ft/sec. The pipe expands to a 4-inch diameter pipe. Find the velocity in the 4-inch diameter pipe.
  - By the Continuity Equation:

$$\mathbf{V}_1 \mathbf{A}_1 = \mathbf{V}_2 \mathbf{A}_2$$



### **Continuity Equation**

#### Example:

Find the cross-sectional area of flow at points 1 and 2 (assume that the pipe is flowing full).

$$A_{1} = \frac{\pi D_{1} 2}{4} = \frac{\pi (2in)(1ft/12in)^{2}}{4} = 0.022 ft^{2}$$
$$A_{2} = \frac{\pi D_{2} 2}{4} = \frac{\pi (4in)(1ft/12in)^{2}}{4} = 0.086 ft^{2}$$

Substituting:

 $V_1 A_1 = V_2 A_2$ (16 ft/sec)(0.022 ft<sup>2</sup>) = V\_2(0.086 ft<sup>2</sup>) V\_2 = 4.09 ft/sec

#### Momentum Equation

- This is a vector relationship, i.e., the force equation may act in more than one direction (x-component, y-component, and possible z-component).
- The Law of Conservation of Momentum:
  - The time rate of change in momentum (defined as the mass rate of flow  $\rho AV$  multiplied by the velocity V) along the path of flow will result in a force called the impulse force.
- Net force on a fluid caused by the change in momentum:

$$F = M(V_2 - V_1) = \rho Q(V_2 - V_1)$$
  
ere F = net force  
M = mass flow rate =  $\rho Q$ 

$$V = velocity$$

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Q =flow rate

 $\rho = density$ 

#### Momentum Equation

#### Example:

Determine the force exerted by the nozzle on the pipe shown when the flow rate is  $0.01 \text{ m}^3/\text{sec}$ . Neglect all losses.



Assume the fluid is water. Need to find velocities using continuity equation. Need cross-sectional area of flow for continuity equation.

## **Momentum Equation**

Solution:

Area at point 1:

$$A_1 = \frac{\pi D_1^2}{4} = \frac{\pi (0.1m)^2}{4} = 0.007854m^2$$

Area at point 2:

$$A_2 = \frac{\pi D_2^2}{4} = \frac{\pi (0.025m)^2}{4} = 0.000491m^2$$

### **Momentum Equation**

#### Solution:

Velocity at point 1:

 $Q_1 = Q = A_1 V_1 = 0.01 m^3 / \text{sec} = (0.007854 m^2) V_1$  $V_1 = 1.273 m / \text{sec}$ 

Velocity at point 2:

 $V_{2} = \frac{Q}{A_{2}} = \frac{0.01m^{3}/\text{sec}}{0.000491m^{2}}$  $V_{2} = 20.37m/\text{sec}$ 

## Momentum Equation

Solution:

Calculating the net force caused by a change in momentum:

 $F = \rho Q(V_2 - V_1)$   $F = (998.2kg / m^3)(0.01m^3 / \sec)(20.37 - 1.273m / \sec)$  $F = 190.6kg - m / \sec^2 = 190.6N$ 

After looking at significant figures: F = 190 N

### **Momentum Equation**

• Momentum equation usually applied to determining forces on a pipe in a bend.



From: Metcalf & Eddy, Inc. and George Tchobanoglous. *Wastewater* Engineering: Collection and Pumping of Wastewater. McGraw-Hill, Inc. 1981.

#### **Momentum Equation**

Equation for the force in the x-direction:

 $F_x = p_2 A_2 \cos\theta - p_1 A_1 + \rho Q (V_2 \cos\theta - V_1)$ 

Equation for the force in the y-direction:  $F_y = p_2 A_2 sin\theta + \rho Q V_2 sin\theta$ 

If the y-direction is vertical, the weight of the water and the pipe will need to be added to the right side of the  $F_y$  equation.

#### Momentum Equation

#### Example:

• Determine the magnitude and direction of the force needed to counteract the force resulting from the change in momentum in a horizontal 90° bend in a 200-mm force main. The rate of flow through the force main is 0.1 m<sup>3</sup>/sec.



Note: The x-y plane is horizontal in this example with equal gravitation forces on all sections of pipe.

#### Momentum Equation

Solution:

• By continuity, the flow rate does not change. Therefore,  $Q = V_1A_1 = V_2A_2$ . The problem indicates that at both points 1 and 2, the diameter is 0.20 m.

Therefore,  $A_1 = A_2$ , and by continuity  $V_1 = V_2$ .

Also given: D = 0.20 m  $\theta = 90^{\circ}$ Looking up:  $\rho = 998.2 \text{ kg/m}^3$  at 20°C (assume T)  $\gamma = 9789 \text{ kg/m}^2\text{-sec}^2$  at 20°C

#### Momentum Equation

Find the cross-sectional area of flow:

$$A = \left(\frac{\pi}{4}\right)D^2 = \left(\frac{\pi}{4}\right)(0.20m)^2$$
$$A = 0.0314m^2$$

Find the velocity of flow:

$$V = \frac{Q}{A} = \frac{0.10m^3/\sec}{0.0314m^2}$$
$$V = 3.18m/\sec$$

#### Momentum Equation

Find the pressure (convert velocity into an energy head term which equals the pressure head term):

By Bernoulli's equation:

$$\frac{p_1}{\gamma} = \frac{v_1^2}{2g}$$
Substituting:
$$\frac{p_1}{\gamma} = \frac{(3.18m/\sec)^2}{2g}$$

$$9789kg / m^2 - \sec^2 - 2(9.81m / \sec^2)$$

 $p_1 = 5045.4 \text{ kg/m-sec}^2 = 5045 \text{ Pa}$ 

### Momentum Equation

Since the pressure in the system is based only on a velocity component at both points 1 and 2,  $p_1 = p_2$ . Since  $V_1 = V_2$  and  $A_1 = A_2$  by continuity (and same diameter pipe on both sides of the bend) and since  $p_1 = p_2$ , simplify the force equations:

 $F_{x} = pAcos\theta - pA + \rho Q(Vcos\theta - V)$   $F_{x} = pA(cos\theta - 1) + \rho QV(cos\theta - 1)$  $F_{x} = (pA + \rho QV)(cos\theta - 1)$ 

 $F_{y} = pAsin\theta + \rho QVsin\theta$  $F_{y} = (pA + \rho QV)sin\theta$ 

#### Momentum Equation

Substituting:

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(pA + \rho QV) = \left[ \left( 504.5kg / m - \sec^2 \right) \left( 0.0314m^2 \right) + \left( 998.2kg / m^3 \right) \left( 0.10m3 / \sec \right) \left( 3.18m / \sec \right) \right] 
(pA + \rho QV) = 475.8kg - m / \sec^2 = 475.8N
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\cos \theta = \cos(90^{\circ}) = 0\sin \theta = \sin(90^{\circ}) = 1
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 $F_x = (475.8N)(0-1)$   $F_x = -475.8N$   $F_y = (475.8N)(1)$  $F_x = 475.8N$ 

Therefore, a thrust block capable of resisting 480 N (sig figs) must be placed against the pipe in both the x-direction and the y-direction and pipe hangers or appropriate bedding will be required to support the pipe from downward gravitational forces.







## Bernoulli's Equation (aka Energy Equation)

For Fluid Flow Between Two Points (in a pipe or channel):

$$\frac{P_1}{\gamma} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\gamma} + \frac{V_2^2}{2g} + z_2 + h_{f_{1-2}}$$

Where  $P/\gamma =$  pressure head

 $V^2/2g =$  velocity head

z = static head

 $h_{f_{1-2}}$  = head loss between two points (usually resulting from shear stress along walls of pipe, within fluid, and from momentum changes at entrances, exits, changes in cross-section or direction, and fittings) – also abbreviated  $H_1$  or  $h_1$ .

**Friction Slope** = rate at which energy is lost along length of flow (channel or pipe)

## Bernoulli's (Energy) Equation



**Hydraulic Grade** = pressure head + elevation head **Energy Grade** = hydraulic grade + velocity head

#### Bernoulli's Equation



From: Terence McGhee. *Water Supply and Sewerage, Sixth Edition.* McGraw-Hill, Inc., New York, NY. 1991.

#### Comparison of Bernoulli's Equation for Pipe Flow vs. Open-Channel Flow



From: Metcalf & Eddy, Inc. and George Tchobanoglous. *Wastewater* Engineering: Collection and Pumping of Wastewater. McGraw-Hill, Inc. 1981.

#### Bernoulli's Equation

Example:

• Water is flowing through a 2-inch pipe at a velocity of 16 ft/sec. The pipe expands to a 4-inch pipe. Given that the pressure in the 2-inch pipe is 40 psig. What is the pressure in the 4-inch pipe just after expansion, assuming that friction is negligible?

Given:

 $V_1 = 16 \text{ ft/sec}$  $g = 32.2 \text{ ft/sec}^2$  $\gamma = 62.4 \text{ lbf/ft}^3$ 



Solving the Continuity Equation earlier,  $V_2 = 4.1$  ft/sec

#### Bernoulli's Equation

#### Example:

Since the centerline does not change elevation  $z_1 = z_2$ , and z's cancel out.

Since friction is negligible,  $h_{f_{1-2}}$  is negligible (set equal to zero). Substituting:

$$\frac{40 \, lb_f / in^2 (12 \, in/ft)^2}{62.4 \, lb_f / ft^3} + \frac{(16 \, ft/sec)^2}{2(32.2 \, ft/sec^2)} = \frac{P_2 (12 \, in/ft)^2}{62.4 \, lb_f / ft^3} + \frac{(4.1 \, ft/sec)^2}{2(32.2 \, ft/sec^2)}$$

$$92.31 \, ft + 3.98 \, ft = (2.31 \, in^2 - ft/lb_f) P_2 + 0.26 \, ft$$

$$96.03 \, ft = (2.31 \, in^2 - ft/lb_f) P_2$$

$$96.03 = (2.31 \, in^2 / lb_f) P_2$$

$$P_2 = 41.57 \, lb_f / in^2 = 41.6 \, psig$$

#### Bernoulli's Equation

Example:

What is the pressure at a depth of 300 feet in fresh water?

Elevation (Depth) Head = 300 feet From Bernoulli's Equation, look at pressure term (all energy is the potential to do work as expressed by the pressure head term): Pressure Head =  $P/\gamma$ 

For water,  $\gamma = 62.4 \text{ lb}/\text{ft}^3$ 

Substituting:

$$300 ft = \frac{P}{62.4lb_f / ft^3}$$

$$P = (18720lb_f / ft^2)(1ft^2 / 144in^2)$$

$$P = 130lb_f / in^2 = 130 psi$$

#### Bernoulli's Equation

#### Example:

What is the theoretical velocity generated by a 10-foot hydraulic head?

From Bernoulli's Equation, look at velocity term (expresses kinetic energy in system): Velocity Head =  $V^{2}/2g$ 

 $g = 32.2 \text{ ft/sec}^2$ 

Substituting:

$$10 ft = \frac{V^2}{2(32.2 ft/sec^2)}$$
$$V^2 = 10 ft(2)(32.2 ft/sec^2) = 644 ft^2/sec^2$$
$$V = 25.4 ft/sec$$

Bernoulli's Equation including Pumps in the System

$$\frac{p_1}{\gamma} + \frac{V_1^2}{2g} + z_1 + E_{pump} = \frac{p_2}{\gamma} + \frac{V_2^2}{2g} + z_2 + h_{f_{1-2}}$$

where  $E_{pump}$  = net energy supplied by the pump (expressed as a head) and includes head losses within the pump

#### Bernoulli's Equation

#### • Example:

A 1200-mm diameter transmission pipe carries 126 L/sec from an elevated storage tank with a water surface elevation of 540 m. Two kilometers from the tank, at an elevation of 434 m, a pressure meter reads 586 kPa. If there are no pumps between the tank and meter location, what is the rate of head loss in the pipe? (Note: 1 kPa = 1000  $N/m^2$ ).

# Bernoulli's Equation

- Solution:
  - Assume: velocity in tank is negligible (valid since the rate of water drawdown at any time is slow compared to the volume of the tank).
  - Assume: pressure head in tank is zero since it is likely open to the atmosphere and the reading on the pressure meter is gauge pressure not absolute pressure.
  - Have pipe diameter and flow rate, so can calculate velocity.

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$$Q = 126L/\sec(1m^3/1000L) = 0.126m^3/\sec(1m^3/1000L)$$

$$A = \frac{\pi}{4}D^2 = \frac{\pi}{4}(1.2m)^2 = 1.13m^2$$
$$V = \frac{Q}{A} = \frac{0.126m^3/\text{sec}}{1.13m^2} = 0.11m/\text{s}$$

# Bernoulli's Equation

- Solution:
  - Check velocity head in pipe.

$$\frac{V^2}{2g} = \frac{0.11m/\sec}{2(9.81m/\sec^2)} = 0.0006m$$

- Substitute into energy equation.

$$\frac{P_1}{\gamma} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\gamma} + \frac{V_2^2}{2g} + z_2 + h_{f_{1-2}}$$
  

$$0m + 0m + 540m = \frac{586,000N/m^2}{9,810N/m^3} + 0m + 434m + h_f$$
  

$$h_f = H_L = 46.27m$$
  
Friction Slope =  $46.27m/2000m \approx 2.3\%$